

An aerial photograph of a city, likely Osaka, Japan, showing a large university campus with several buildings and green spaces. The text is overlaid on the image.

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**Biotechnology Advanced  
Environmental Biotechnology**

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**Keep water clean!**

# Environmental Biotechnology

1. Water quality and pollution
2. Wastewater treatment

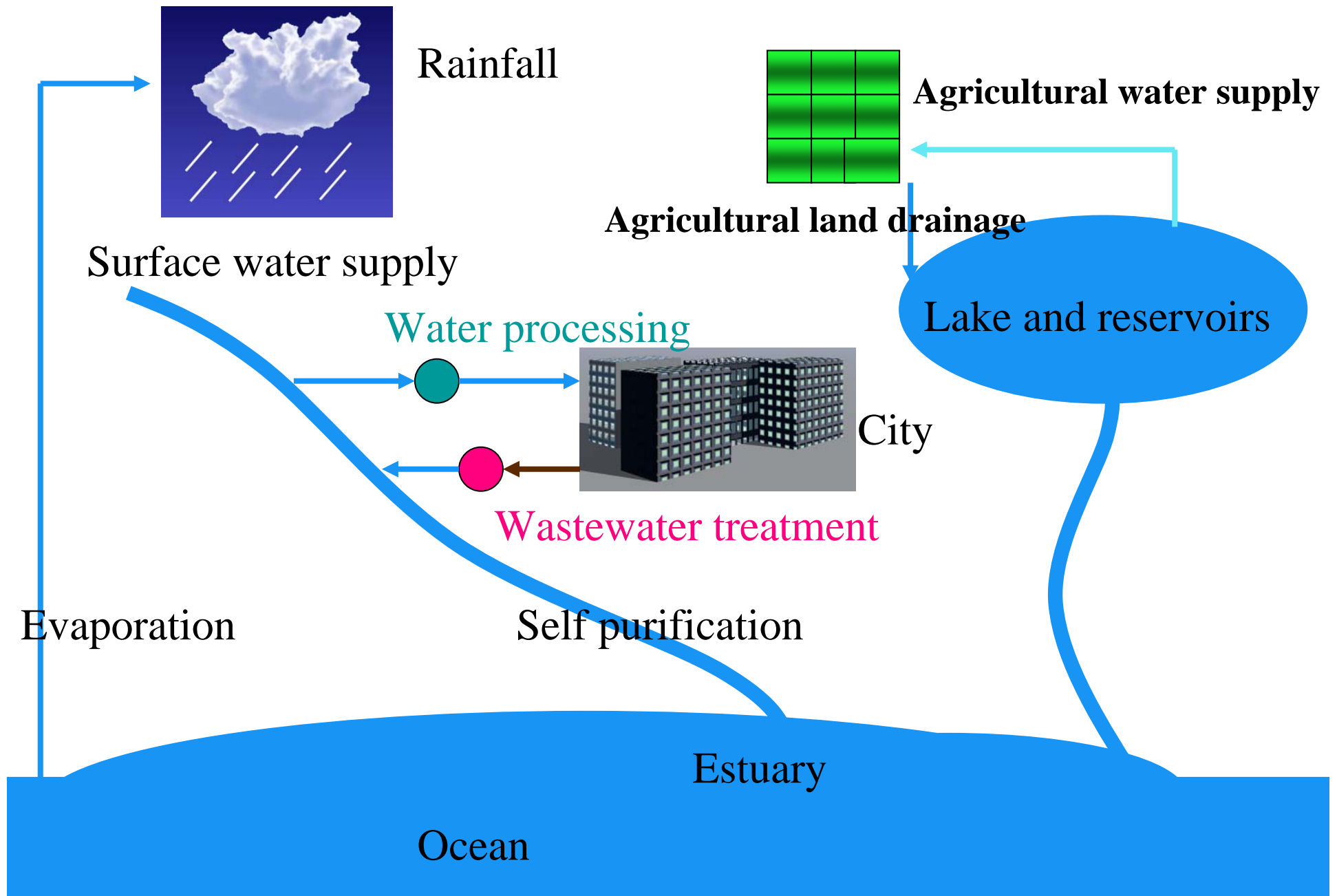
# Water quality and pollution

- Introduction
- Stream and self-purification
- Eutrophication

# **Water quality and pollution**

- Introduction

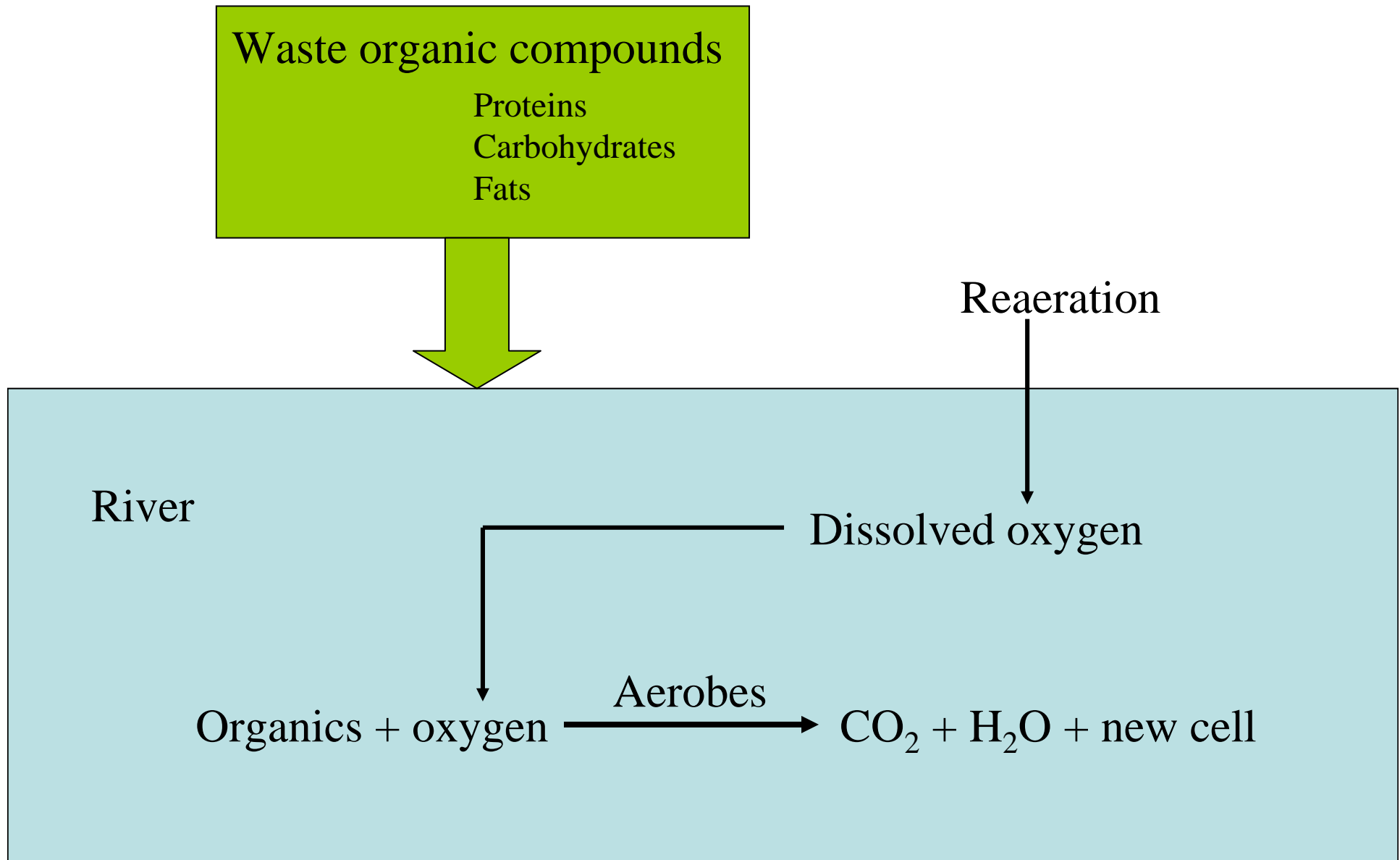
# The integration of natural and man-generated water cycle



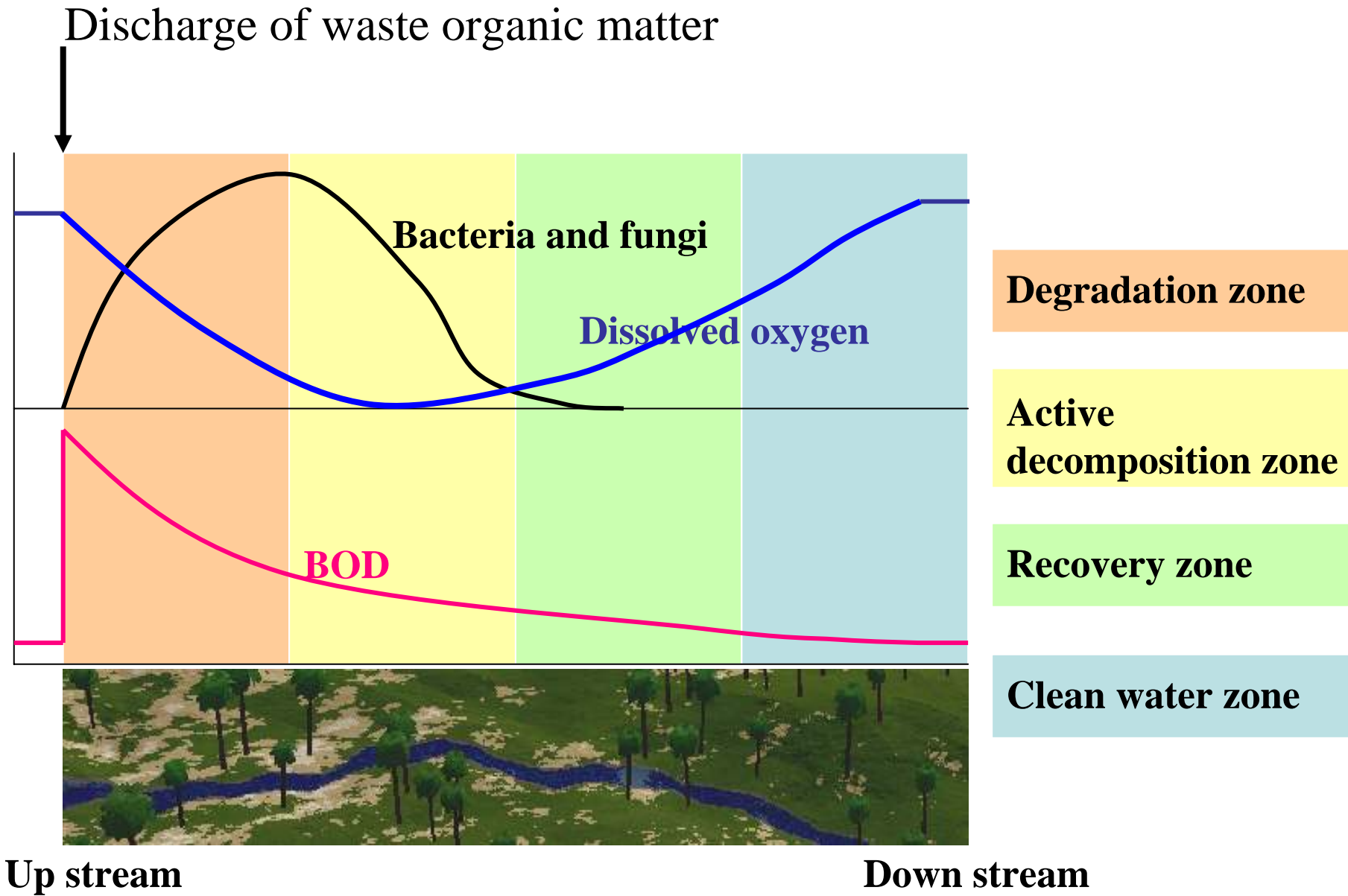
# **Water quality and pollution**

- Stream pollution and self-purification

# Stream pollution and self-purification



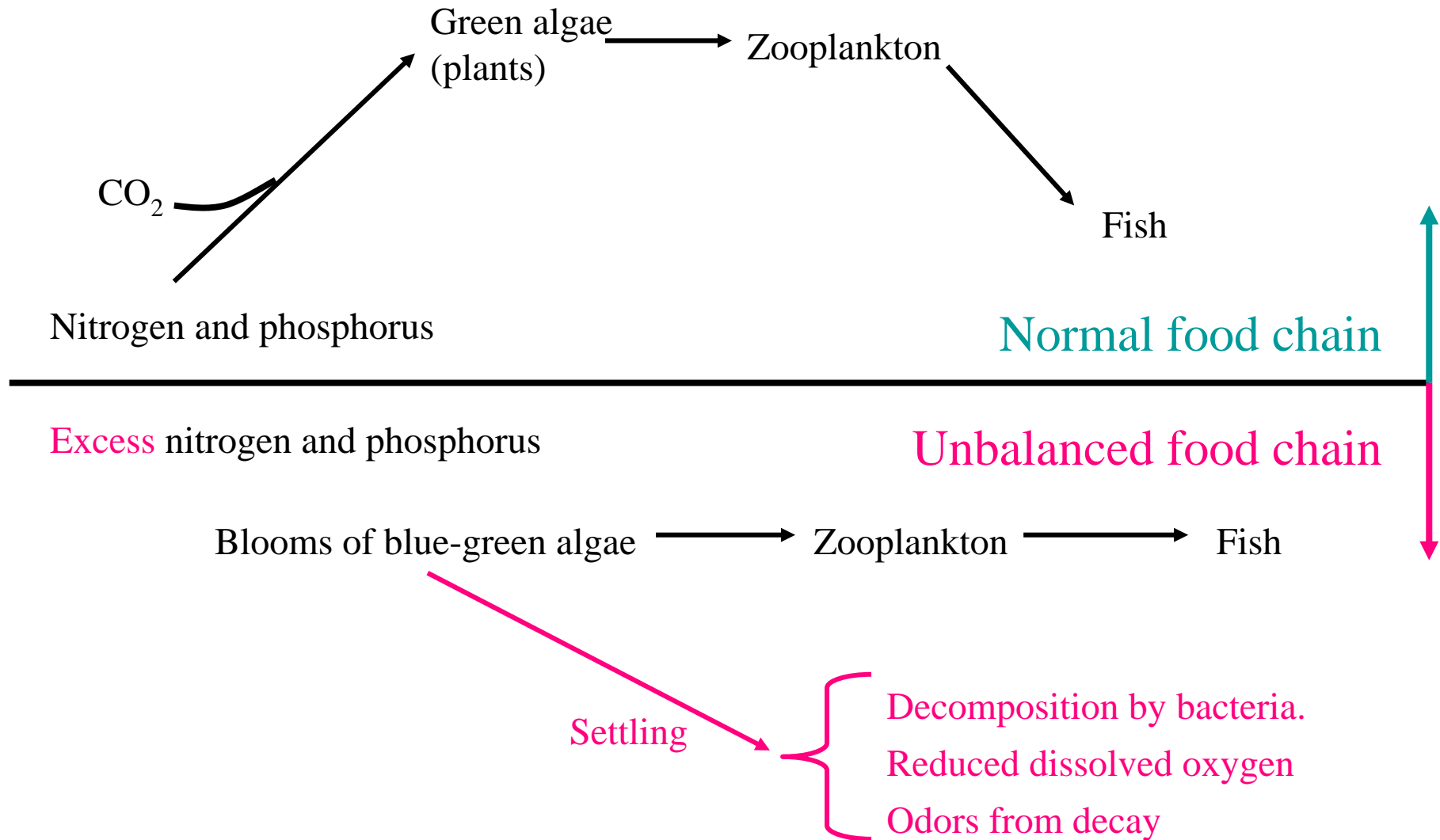




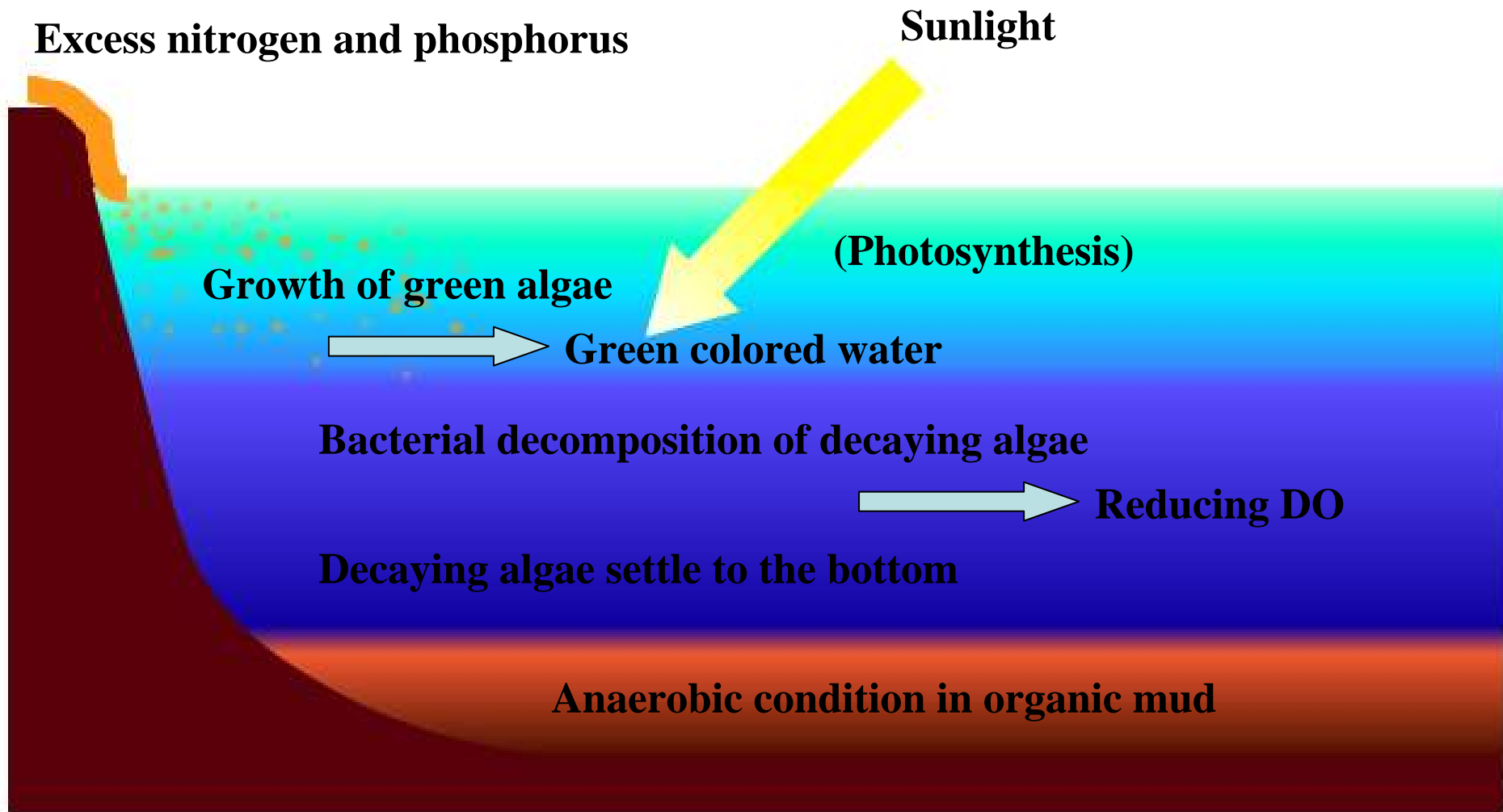
Effect of organic pollution and self-purification on a stream.

# **Water quality and pollution**

- Eutrophication



Aquatic food chain unbalanced by eutrophication compared with normal chain



# Eutrophic lake

- The accepted upper limits for lakes free of algal blooms

( Ammonia + Nitrate )-N      0.3 mg/l

Orthophosphate-P              0.02 mg/l

- Lakes will exhibit algal blooms

Total-N                              0.8 mg/l

Total-P                              0.1 mg/l

# Biological treatment systems

Activated sludge process

Advanced wastewater treatment

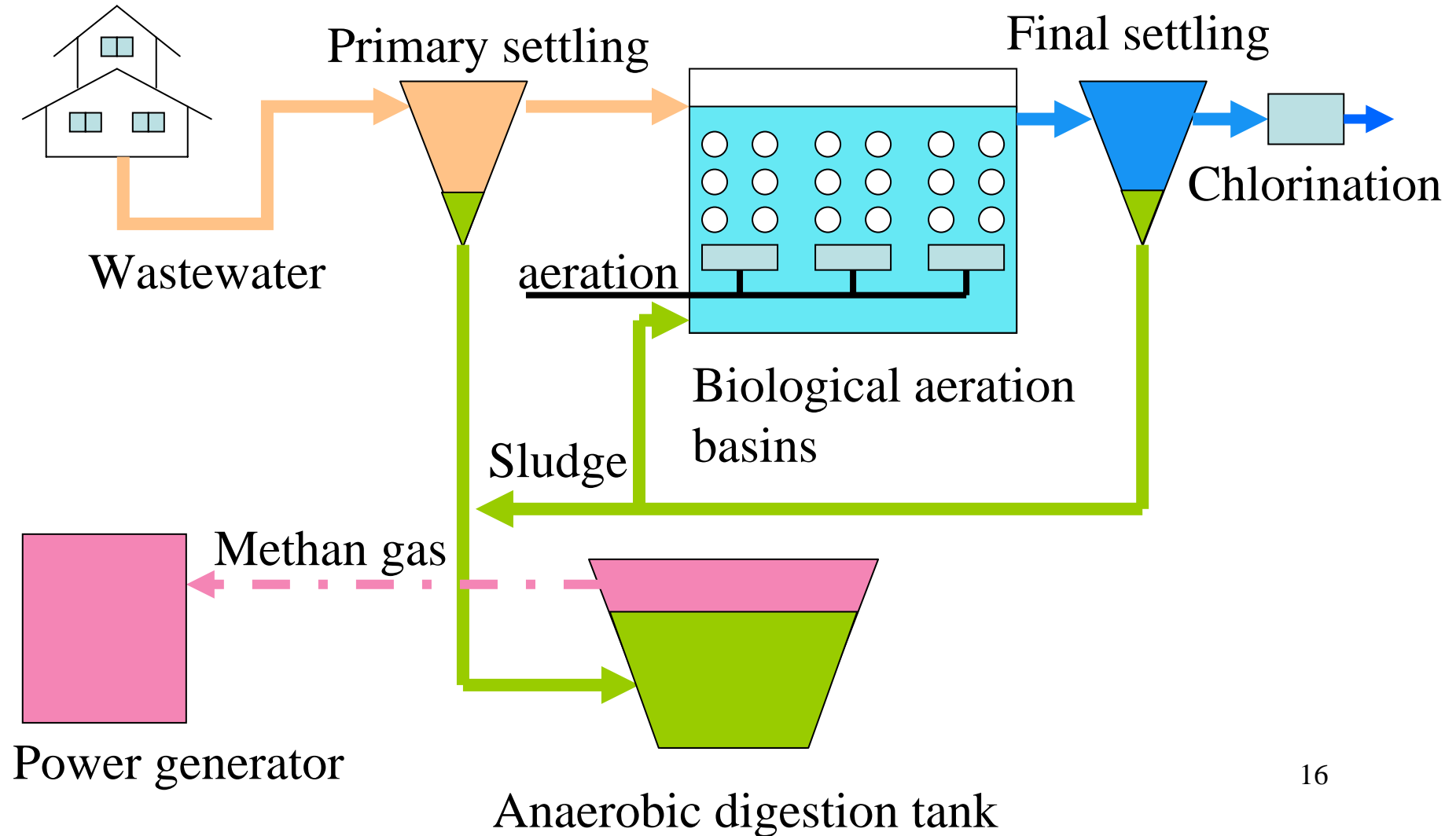
- Biological nitrogen removal
- Biological phosphorus removal

# Biological treatment systems

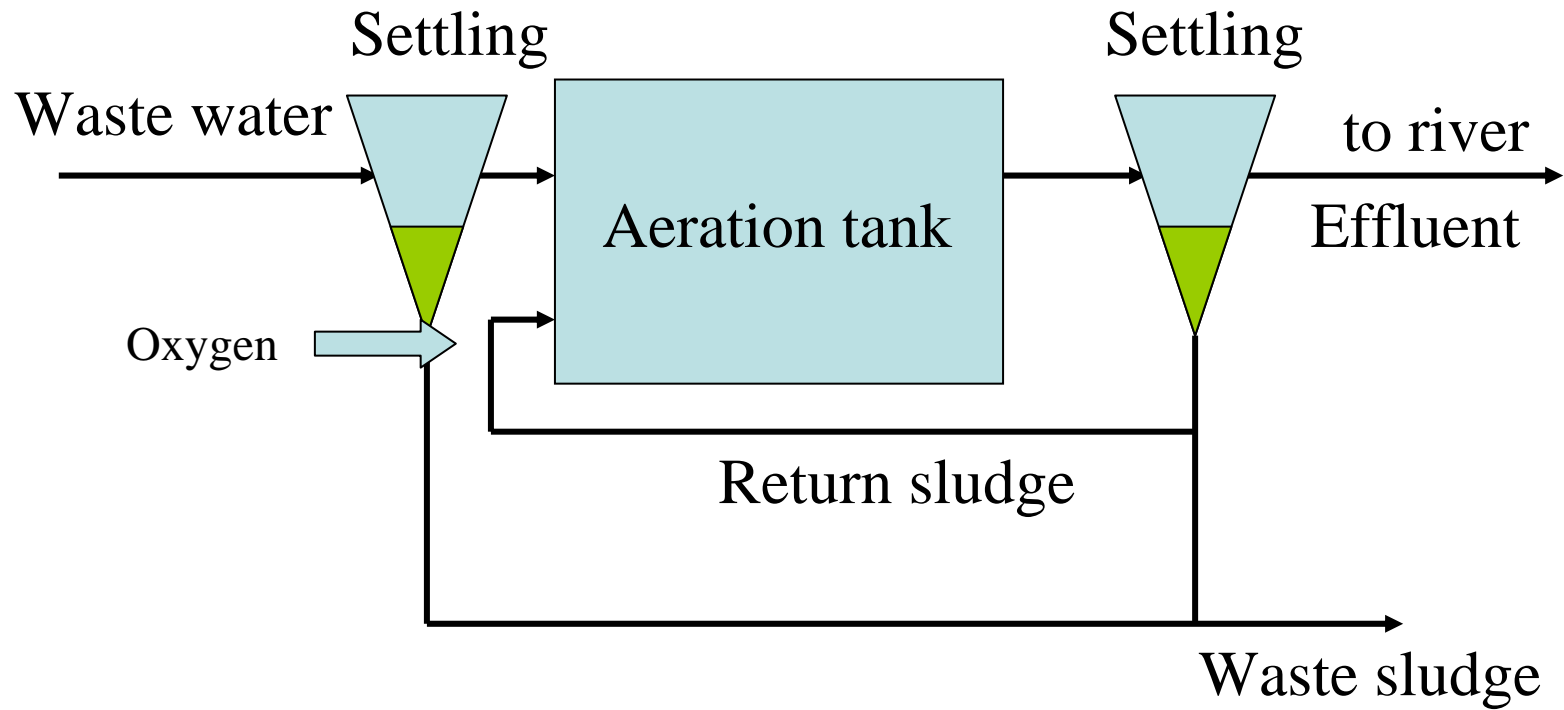
## Activated sludge process

# Biological treatment

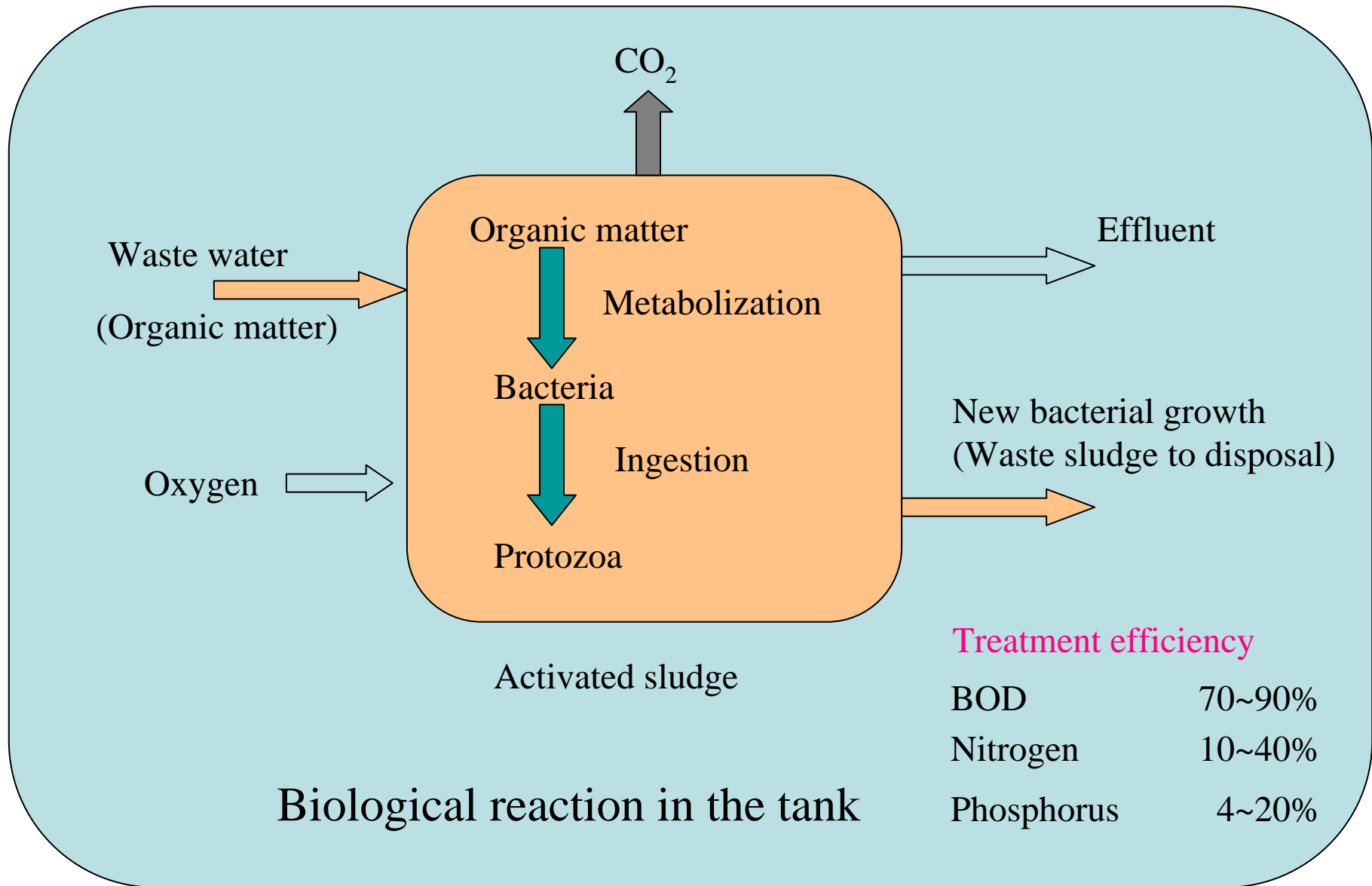
## 1. Activated sludge process







Waste water treatment by activated sludge system



Waste water treatment by activated sludge system

# **Design of activated sludge process**

**Kinetics of biological growth**

**Application of kinetics to wastewater treatment systems**

.

# Design of activated sludge process

## Kinetics of biological growth

$$\left[ \frac{dX}{dt} \right]_{grow} = Y \left[ \frac{dS}{dt} \right]_{con} - k_d X \quad (1)$$

$\left[ \frac{dX}{dt} \right]_{grow}$  = net growth rate of microorganisms

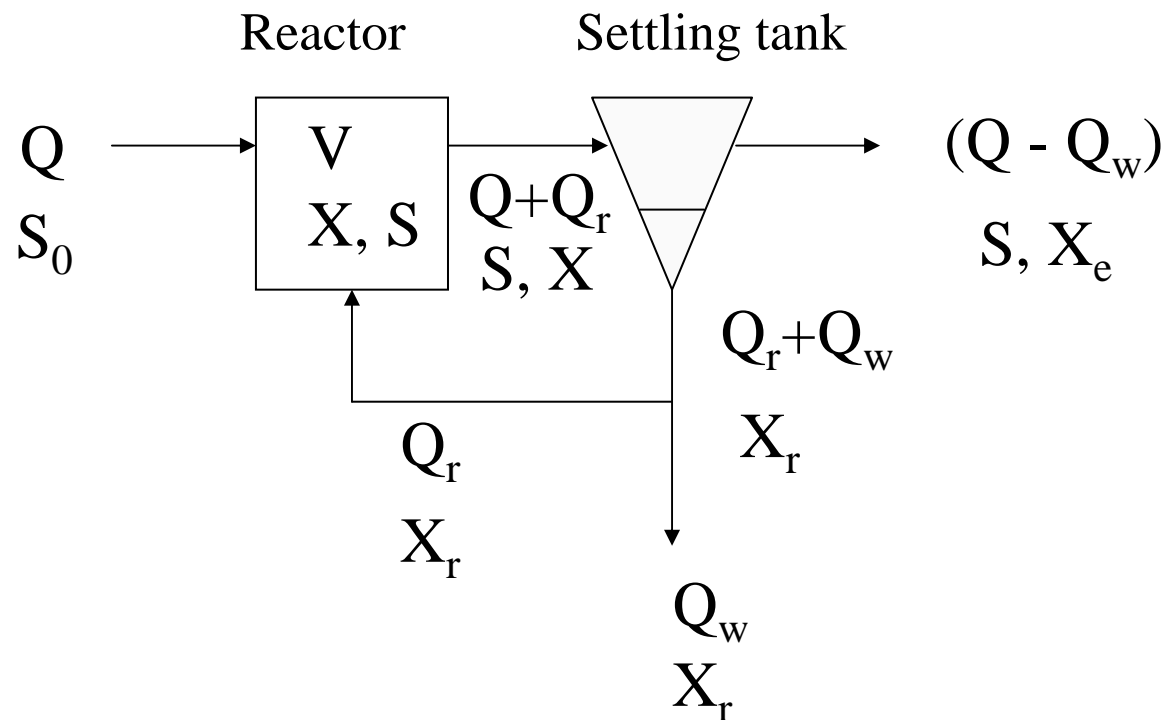
$\left[ \frac{dS}{dt} \right]_{con}$  = rate of BOD utilization by microorganisms

$k_d$  = microorganisms decay constant

$Y$  = growth yield coefficient,

mass of microorganism / mass BOD utilized<sub>20</sub>

# Application of kinetics to treatment system



Schematic of an activated sludge reactor with sludge recycle

A material balance for the mass of cells in the entire system can be written as

$$\begin{aligned} \left[ \begin{array}{l} \text{Rate of change} \\ \text{of cells} \\ \text{concentration} \\ \text{in reactor} \end{array} \right] &= \left[ \begin{array}{l} \text{Net rate of} \\ \text{cells growth} \\ \text{in reactor} \end{array} \right] - \left[ \begin{array}{l} \text{Rate of cells} \\ \text{outflow} \\ \text{from reactor} \end{array} \right] \\ V \left( \frac{dX}{dt} \right) &= \left( Y \left( \frac{dS}{dt} \right)_{con} - k_d X \right) V - (Q_w X_r + (Q - Q_w) X_e) \end{aligned} \quad (2)$$

$Y$  : growth yield coefficient, mass of cells / mass BOD utilized

$k_d$  : cells decay coefficient

$X$  : the concentration of cells in the reactor

$X_e$  : the concentration of cells in the effluent

$X_r$  : the concentration of cells in the recycle flow

$Q_w$  : the cell-wasting rate.

$$\left( \frac{dS}{dt} \right)_{con} = \text{consumption rate of BOD}$$

At steady state,  $dX/dt$  equals 0, Eq. (2) can be rewritten as

$$(Q_w X_r + (Q - Q_w) X_e) = \left( Y \left( \frac{dS}{dt} \right)_{con} - k_d X \right) V \quad (3)$$

In a system with a properly operating settling units, the concentration of the cells in the effluent,  $X_e$  is very small, Eq. (3) can be simplified to give

$$Q_w X_r = \left( Y \left( \frac{dS}{dt} \right)_{con} - k_d X \right) V \quad (4)$$

Dividing both sides of Eq. (4) by  $XV$  gives

$$\frac{Q_w X_r}{XV} = \left( \frac{Y}{X} \left( \frac{dS}{dt} \right)_{con} - k_d \right) \quad (5)$$

The mean cell residence time  $\theta_c$  is defined as

$$\theta_c = \frac{XV}{Q_w X_r} \quad (6)$$

The mean hydraulic retention time  $\theta$  for the reactor is defined as

$$\theta = \frac{V}{Q} \quad (7)$$

where,

$V$  : the volume of the reactor

$Q$  : the flow rate of waste water to the reactor

.



Eq.(5) can be simplified

or

$$\frac{1}{\theta_c} = Y \left( \frac{\left( \frac{dS}{dt} \right)_{con}}{X} \right) - kd \quad (8)$$

where,

$$\frac{1}{\theta_c} = Y \nu - k_d \quad (9)$$

$$\nu = \frac{\left( \frac{dS}{dt} \right)_{con}}{X}$$

$\nu$  is commonly known as the specific BOD consumption rate or specific waste removal rate.

The waste removal rate in the reactor can be evaluated,

$$V \left( \frac{dS}{dt} \right)_{con} = Q(S_0 - S) \quad (10)$$

Using Eqs. (6), (7) and (10), the cell concentration  $X$  in the reactor can be obtained,

$$X = \frac{\theta_c Y (S_0 - S)}{\theta (1 + k_d \theta_c)} \quad (11)$$

Sludge production rate,  $R_s$  can be calculated by using Eq. (6)

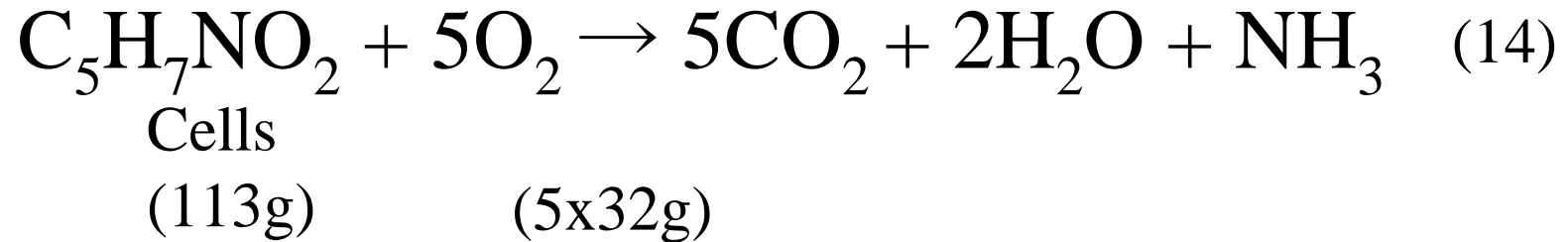
$$R_s = Q_w X_r = \frac{XV}{\theta_c} \quad (12)$$

## Oxygen requirements

The theoretical oxygen requirement can be calculated by knowing BOD of wastewater and the amount of organisms wasted from the system.

$$O_2 \left( \frac{g}{day} \right) = \left[ \begin{array}{l} \text{BOD utilized} \\ \text{per day} \end{array} \right] - \left[ \begin{array}{l} \text{BOD of organisms} \\ \text{wasted per day} \end{array} \right] \quad (13)$$

The BOD of a mole of cells is assumed as follows,



$$\frac{O_2}{\text{cells}} = \frac{160}{113} = 1.42 \left( \frac{g \ O_2}{g \ - \ cell} \right) \quad (15)$$

Consequently, the BOD of cells is equal to

$$\text{BOD} = 1.42(\text{cells}) \quad (16)$$

Therefore, the theoretical oxygen requirement for an activated sludge system can be calculated as

$$O_2 \left( \frac{g}{day} \right) = \left[ \begin{array}{l} \text{BOD utilized} \\ \text{per day} \end{array} \right] - 1.42 \left[ \begin{array}{l} \text{organisms} \\ \text{wasted per day} \end{array} \right] \quad (17)$$

$$O_2 \left( \frac{g}{day} \right) = \left( \frac{dS}{dt} \right)_{con} - 1.42 \left( \frac{dX}{dt} \right)_{gr} \quad (18)$$

$$= Q(S_0 - S) - 1.42 Q_w X_r \quad (19)$$

Then, if the oxygen transfer efficiency of the aeration system is known, the actual air requirement can be determined.

# Advanced wastewater treatment

## Biological nitrogen removal

## Nitrogen content in municipal wastes

4 - 6kg of nitrogen per person per year.

## Common form of nitrogen

organic, ammonia, nitrate and nitrite.

## Decomposition of nitrogenous organic matter

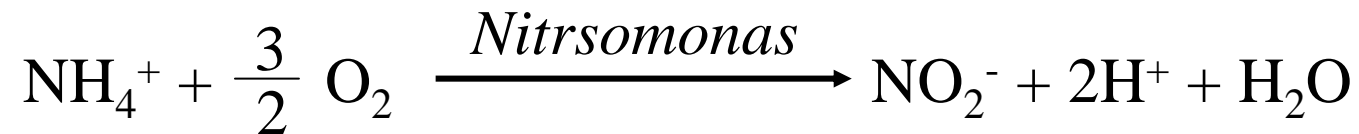
Bacterial decomposition

Organic nitrogen compounds  $\rightarrow$   $\text{NH}_3$

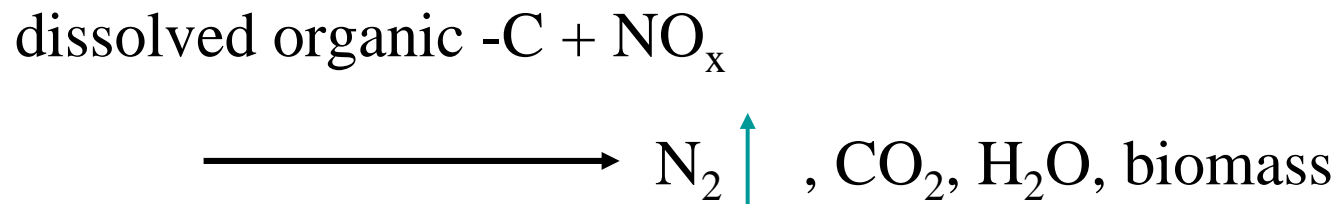
# Advanced wastewater treatment

- Nitrification and nitrogen removal

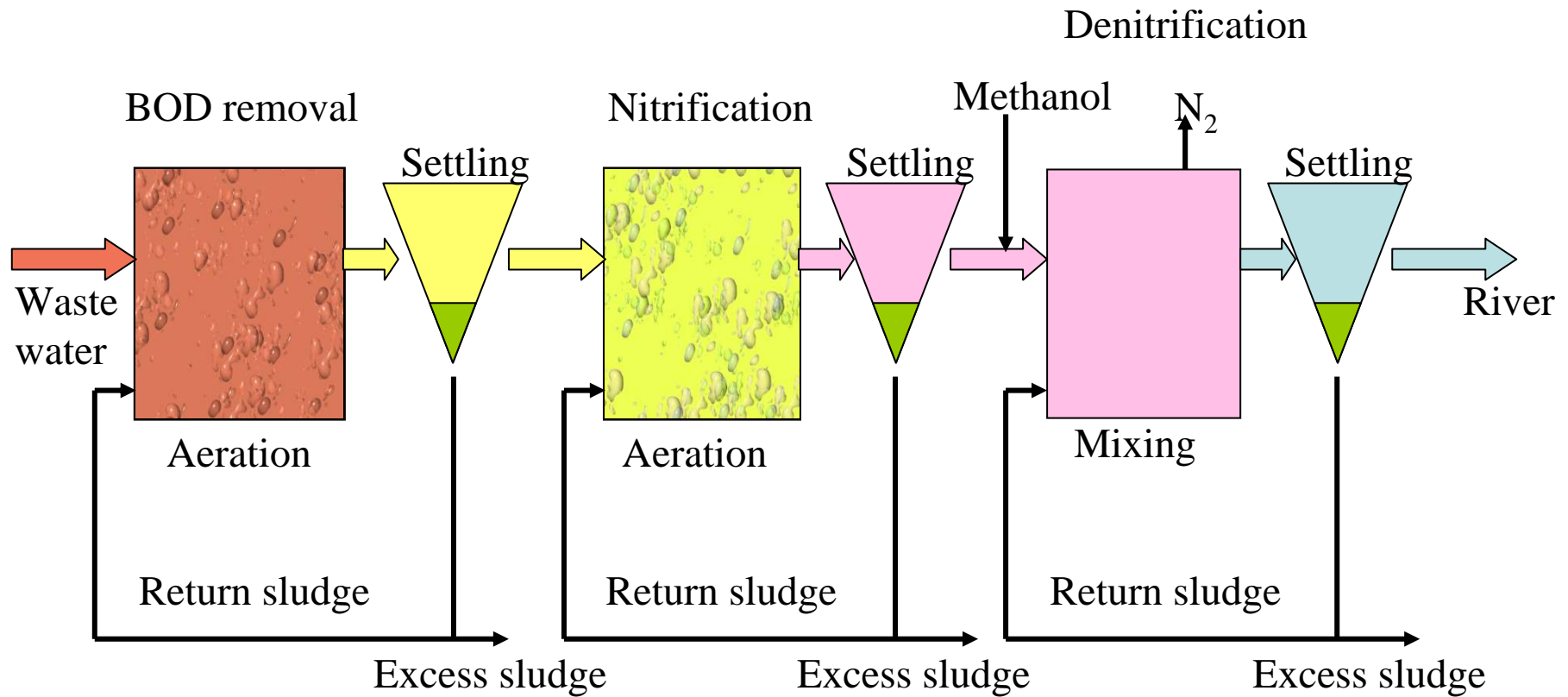
Bacterial nitrification (autotrophic bacteria)



Bacterial denitrification (heterotrophic bacteria)







Advanced waste water treatment by three activated sludge system (Nitrogen removal)

# Treatment efficiency

## Conventional activated sludge process

BOD 70 – 80%

Nitrogen 10 – 40%

## Advanced activated sludge process

BOD 80 - 90%

Nitrogen 60 – 70%

# Advanced wastewater treatment

## Biological phosphorus removal

# Phosphorus content in the cell

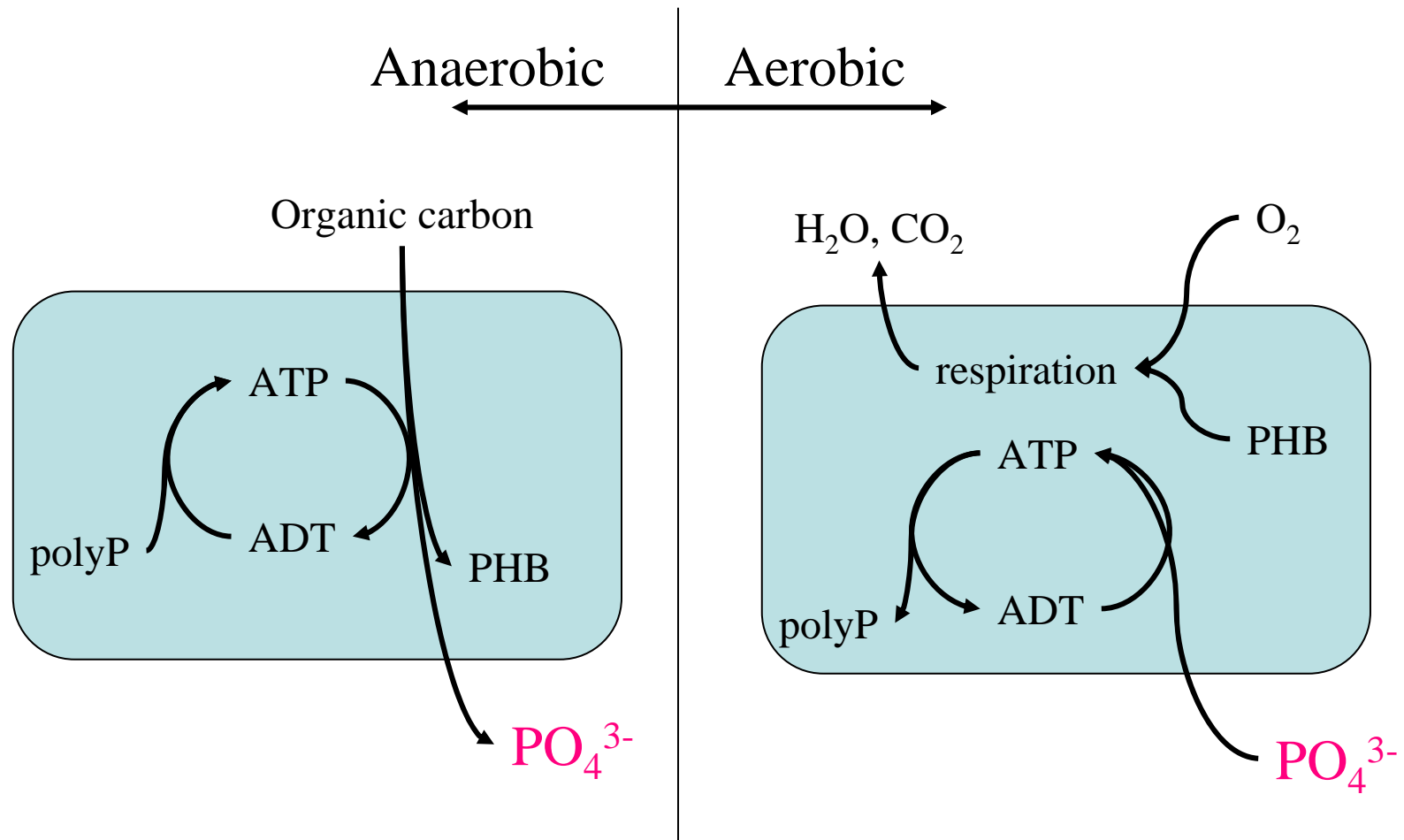
Conventional activated sludge

about 3% of the cell dry mass

Polyphosphate accumulating activated  
sludge bacteria

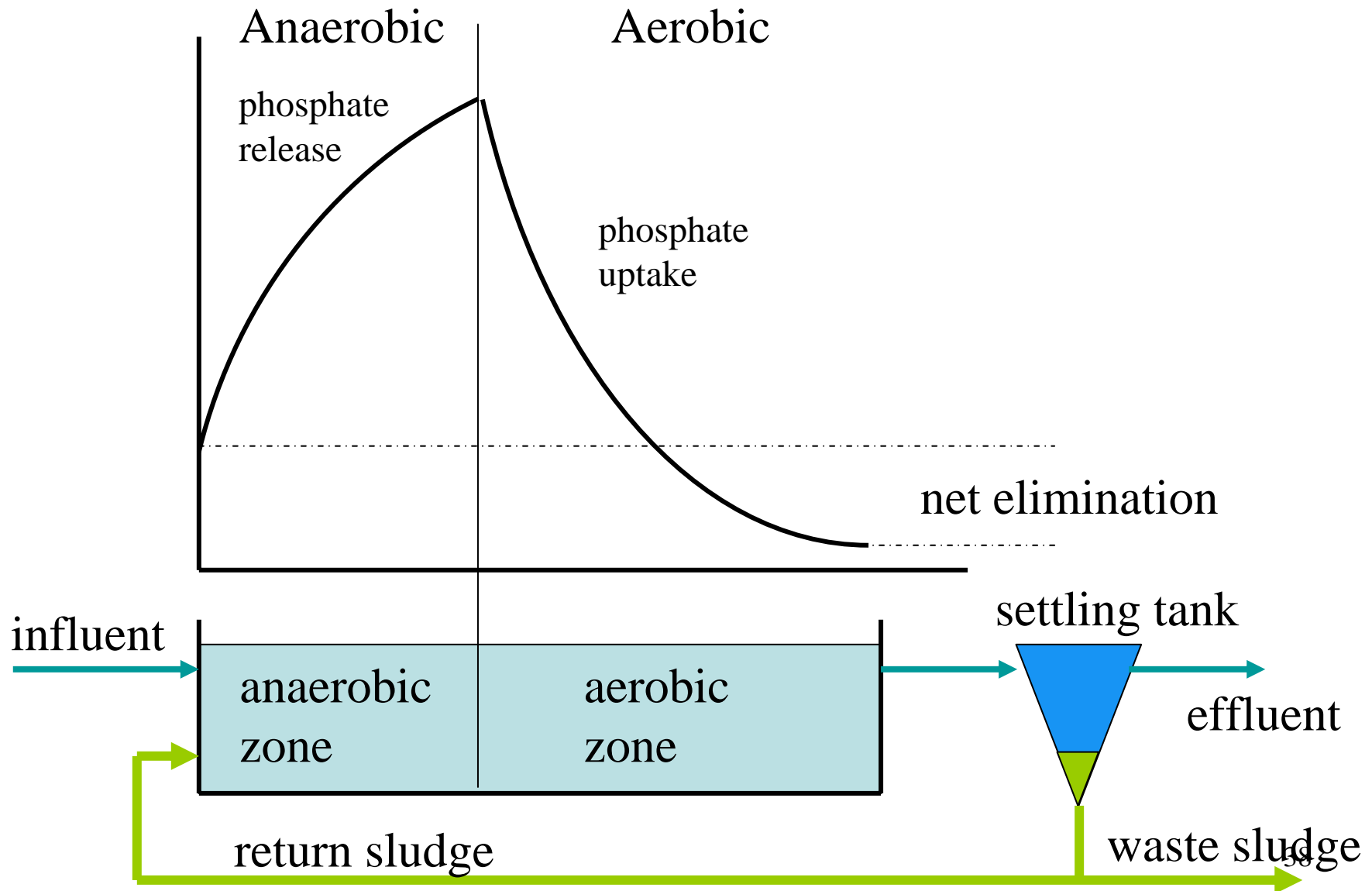
more than 12% of the cell dry mass

# Biochemical model of enhanced phosphorus uptake and release



PHB : poly- $\beta$ -3 hydroxy butyric acid  
polyP : poly phosphate

# Biological phosphorus removal





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**END**

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